



**. . . Fire Protection by Computer Design**

Sprinkler Systems Inc.  
2-4 Avon Street  
P O Box 1285  
Lewiston, Maine 04240  
207-782-0104

Job Name : MURRAY HOUSE  
Building :  
Location : 104 NORTH STREET, PORTLAND, MAINE 04101  
System : 1 OF 1  
Contract : 12111  
Data File : 12111MURRAYHOUSEA1.WXF

HYDRAULIC DESIGN INFORMATION SHEET

Name - MURRAY HOUSE Date - 2-5-2013  
Location - 104 NORTH STREET, PORTLAND, MAINE 04101  
Building - System No. - 1 OF 1  
Contractor - REDFERN PROPERTIES Contract No. - 12111  
Calculated By - SCOTT E. GARLAND Drawing No. - 1,2 OF 2  
Construction: (X) Combustible ( ) Non-Combustible Ceiling Height 8-5  
OCCUPANCY - RESIDENTIAL - SINGLE FAMILY DWELLING

S Type of Calculation: ( )NFPA 13 Residential ( )NFPA 13R (X)NFPA 13D  
Y Number of Sprinklers Flowing: ( )1 (X)2 ( )4 ( )  
S ( )Other  
T ( )Specific Ruling Made by Date  
E  
M Listed Flow at Start Point - 13.0 Gpm System Type  
Listed Pres. at Start Point - 7.0 Psi (X) Wet ( ) Dry  
D MAXIMUM LISTED SPACING 16 x 16 ( ) Deluge ( ) PreAction  
E Domestic Flow Added - Gpm Sprinkler or Nozzle  
S Additional Flow Added - Gpm Make RELIABLE Model F1RES49  
I Elevation at Highest Outlet - 184.0Feet Size 1/2 X 1/2 K-Factor 4.9  
G Note: Temperature Rating 155 DEG  
N DESIGN AREA #1 - 3RD FLOOR OFFICE

Calculation Gpm Required 26.775 Psi Required 39.960 AT BASE OF RISER  
Summary C-Factor Used: Overhead 150 Underground 140

W Water Flow Test: Pump Data: Tank or Reservoir:  
A Date of Test - 3-27-2006 Rated Cap. Cap.  
T Time of Test - @ Psi Elev.  
E Static (Psi) - 44 Elev.  
R Residual (Psi) - 37 Other Well  
Flow (Gpm) - 1518 Proof Flow Gpm  
S Elevation - 157.0

P Location: ON NORTH STREET, APPROXIMATELY 700'-0" FROM THE BUILDING

P  
L Source of Information: PORTLAND WATER DISTRICT  
Y

# Fittings Used Summary

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MURRAY HOUSE

Page 3  
Date 2-5-2013

## Fitting Legend

Abbrev.	Name	½	¾	1	1¼	1½	2	2½	3	3½	4	5	6	8	10	12	14	16	18	20	24
E	NFPA 13 90' Standard Elbow	1	2	2	3	4	5	6	7	8	10	12	14	18	22	27	35	40	45	50	61
Fsp	Flow Switch Potter VSR	Fitting generates a Fixed Loss Based on Flow																			
T	NFPA 13 90' Flow thru Tee	3	4	5	6	8	10	12	15	17	20	25	30	35	50	60	71	81	91	101	121

## Units Summary

Diameter Units           Inches  
 Length Units            Feet  
 Flow Units               US Gallons per Minute  
 Pressure Units          Pounds per Square Inch

# Pressure / Flow Summary - STANDARD

Sprinkler Systems Inc.  
MURRAY HOUSE

Page 4  
Date 2-5-2013

Node No.	Elevation	K-Fact	Pt Actual	Pn	Flow Actual	Density	Area	Press Req.
TYP	0.0	4.9	7.04	na	13.0	0.05	260	7.0
1	184.0	K = K @ DROP	7.35	na	13.0			
2	184.0	K = K @ DROP	8.25	na	13.77			
A	183.0		9.04	na				
B	174.417		14.07	na				
C	174.417		14.76	na				
D	164.5		19.6	na				
E	164.5		19.91	na				
F	154.5		24.81	na				
RT	154.5		25.05	na				
TV	150.5		30.05	na				
RB	146.25		39.96	na				
X1	152.0		39.28	na				
TEST	157.0		37.12	na				

The maximum velocity is 6.33 and it occurs in the pipe between nodes RB and X1

# Final Calculations - Hazen-Williams

Sprinkler Systems Inc.  
MURRAY HOUSE

Page 5  
Date 2-5-2013

Hyd. Ref. Point	Qa Qt	Dia. "C" Pf/Ft	Fitting or Eqv.	Ln.	Pipe Ftng's Total	Pt Pe Pf	Pt Pv Pn	*****	Notes	*****
TYP to DROP	13.00 13.0	1.101 150.0 0.0306	1T	9.563 0.0 0.0	0.500 9.562 10.062	7.039 0.0 0.308			K Factor = 4.90	
	0.0 13.00						7.347		K Factor = 4.80	
1 to 2	13.00 13.0	1.101 150.0 0.0307	2E	7.65 0.0 0.0	21.750 7.650 29.400	7.347 0.0 0.902			K Factor @ node DROP	
									Vel = 4.38	
2 to A	13.77 26.77	1.394 150.0 0.0370	1E	4.762 0.0 0.0	5.000 4.761 9.761	8.249 0.433 0.361			K Factor @ node DROP	
									Vel = 5.63	
A to B	0.0 26.77	1.394 150.0 0.0370	2E 1T	9.523 9.523 0.0	16.250 19.046 35.296	9.043 3.717 1.306				Vel = 5.63
B to C	0.0 26.77	1.598 150.0 0.0190	1T	11.656 0.0 0.0	24.833 11.656 36.489	14.066 0.0 0.694				Vel = 4.28
C to D	0.0 26.77	1.598 150.0 0.0190	1E 1T	5.828 11.656 0.0	11.250 17.484 28.734	14.760 4.295 0.547				Vel = 4.28
D to E	0.0 26.77	1.598 150.0 0.0190	1T	11.656 0.0 0.0	4.583 11.656 16.239	19.602 0.0 0.308				Vel = 4.28
E to F	0.0 26.77	1.598 150.0 0.0190	1E 1T	5.828 11.656 0.0	12.250 17.484 29.734	19.910 4.331 0.566				Vel = 4.28
F to RT	0.0 26.77	1.610 120.0 0.0278		0.0 0.0 0.0	8.750 0.0 8.750	24.807 0.0 0.243				Vel = 4.22
RT to TV	0.0 26.77	1.610 120.0 0.0277	1E 1Fsp	4.0 0.0 0.0	5.667 4.000 9.667	25.050 4.732 0.268			* Fixed loss = 3	Vel = 4.22
TV to RB	0.0 26.77	1.610 120.0 0.0276		0.0 0.0 0.0	2.500 0.0 2.500	30.050 9.841 0.069			* Fixed loss = 8	Vel = 4.22
RB to X1	0.0 26.77	1.314 150.0 0.0493	1E 1T	2.247 4.495 0.0	30.000 6.742 36.742	39.960 -2.490 1.812				Vel = 6.33
X1 to TEST	0.0 26.77	12.34 140.0 0.0		0.0 0.0 0.0	700.000 0.0 700.000	39.282 -2.166 0.001				Vel = 0.07
	0.0 26.77						37.117		K Factor = 4.39	

# Water Supply Curve (C)

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MURRAY HOUSE

Page 6  
Date 2-5-2013

City Water Supply:  
C1 - Static Pressure : 44  
C2 - Residual Pressure: 37  
C2 - Residual Flow : 1518

Demand:  
D1 - Elevation : 11.694  
D2 - System Flow : 26.7745  
D2 - System Pressure : 37.117  
Hose ( Adj City ) : \_\_\_\_\_  
Hose ( Demand ) : \_\_\_\_\_  
D3 - System Demand : 26.7745  
Safety Margin : 6.879

